

Drinking Water Production Using Temperature Swing Solvent Extraction Kem, Diana; Lee, Seungjin

Introduction

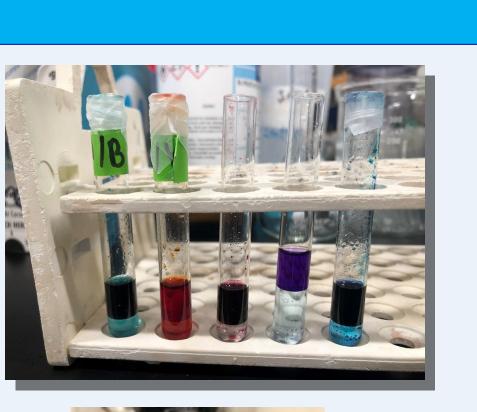
Temperature swing solvent extraction (TSSE) is an effective technique characterized by membrane-less desalination and being a low energy, cost-effective alternative for saline feeds. While the application of TSSE in desalination has been studied, little is known about the effect of different amines on the efficiency of the technology. Through a cycle of temperature swing extraction experiments conducted for each type of amine, product water is extracted and analyzed.

Objectives and Approach

The objective of this research is to focus on the systematic elucidation of the parameters influencing the TSSE. In particular, the comparison of the affinity of secondary and tertiary amines to produce potable water. Various amines were chosen to test the effect of degree of substitution as well as comparisons between amines with similar types of functional groups on the extraction performance.

Methods

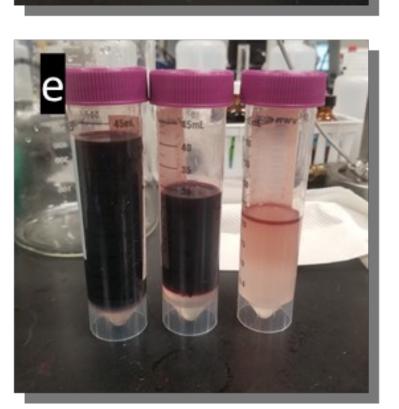
- 1. Dyes to visually demonstrate a clear separation
- 2. TSSE experiments utilizing low and high temperature swing
- 3. Product water analysis: a. Mass of water recovered **b.** Residual salt concentration and amine concentration: **Rotary Evaporator and TOC analyzer**





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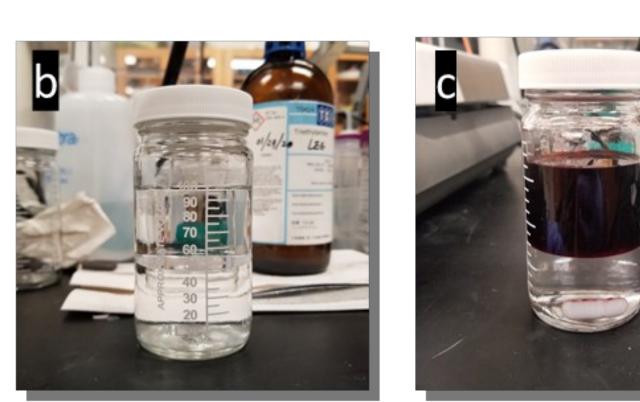
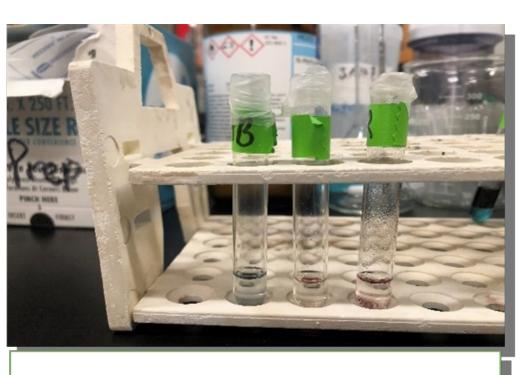


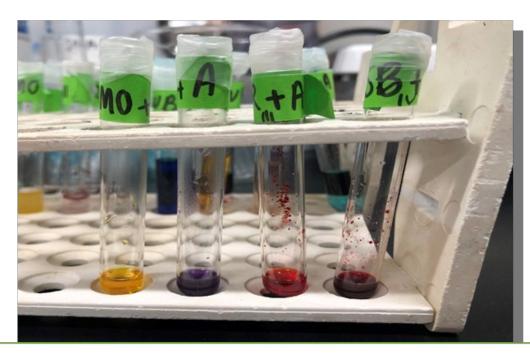


Figure 1. (A) 1 M saline solution (B) Amine added into vial, layers separate (C) Sudan IV red dye added into vial (visualize layers) (D) Low temperature water bath at 16°(E) Amine and water layer and dewatered raffinate (F) Amine and water layer separated (G) High temperature water bath at 68° and (H) Product water extracted





MCHA + Yellow 40, Red 40, Blue 1

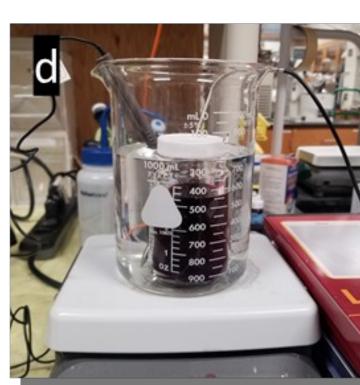


MCHA+ Methylene Orange, Methylene Blue, Sudan III, and Sudan IV.

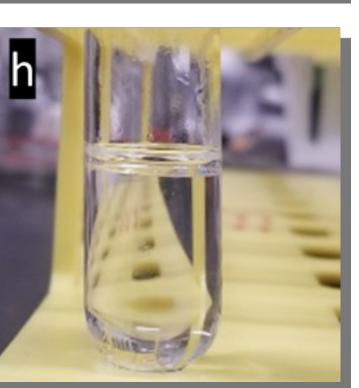
Figure 2. Dye tests ran on amine and water layer for identification.

Table 1. Data of amines that Boo's paper also tested. It consists of two secondary and one tertiary

Amine	Product Water Recovered (g)	Salt Recovered (g)	Concentrated Saline Brine Recovered (mL)
Diisopropylamine	0.8	0.22	~1.6
Diisopropylethylamine	0.1	0.21	~1.8
N,N- Diethylcyclohexylamine	0.2		~2.0







Results

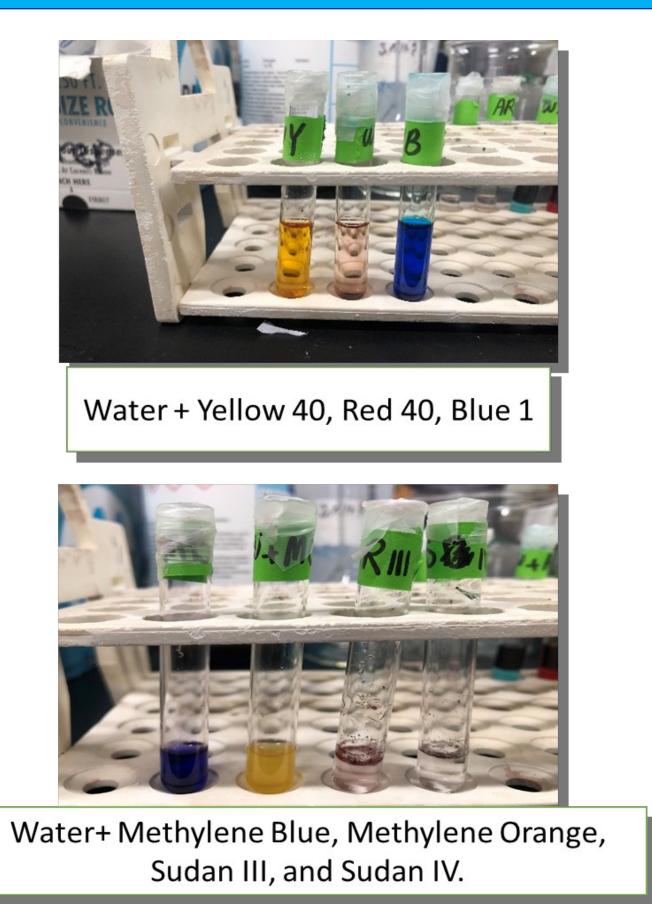


Table 2. Recent amine data that has been scaled up from previous semester.

Amine

Friethylamine N-Ethylcyclohexylamine N-Methylcyclohexylami Diisopropylamine



- identification.
- A larger volume of water was recovered from the extraction with secondary amines using the same volume of solvents. There is also differential affinity of solvents to water with amines containing similar moieties. Lower volumes of saline
- water show a higher amine affinity for water.
- Noticeable differences in the efficiency of water extraction from highly concentrated brine are found for secondary and tertiary amines.

- conducted.
- Conclusive extraction results and analysis of the correlation among parameters will be presented.
- Include additional set of extraction experiments using asymmetric substituents and the optimization of the extraction temperature for individual amines.

References Boo, C., Winton, R. K., Conway, K. M., & Yip, N. Y. (2019). Membrane-less and Non-Evaporative Desalination of Hypersaline Brines by Temperature Swing Solvent Extraction. Environmental Science & Technology Letters, 6(6), 359-364. doi:10.1021/acs.estlett.9b00182

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	Product Water Recovered (g)	Concentrated Saline Brine Recovered (mL)
	2.892	~40.0
e	8.879	~40.0
ine		~25.0
	14.431	~28.0



Figure 3. Comparison between amine water affinity after low temperature water bath. They are N-Ethylcyclohexylamine and N-Methylcyclohexylamine, respectively. Both are secondary structures.

Conclusions

Sudan IV red dye chosen as the most viable option for

Future Work

Further tests with varying experimental conditions to be